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Description

The invention relates to the preparation of a nickel-based catalyst for hydrogenation reactions.

Nickel-based catalysts are well-known and are widely used as hydrogenation catalysts. It is customary to prepare them by precipitating nickel-hydroxide and/or -carbonate from an aqueous solution of a nickel salt using an alkaline reactant, often in the presence of a carrier.

In the preparation of these catalysts measures are often taken to precipitate the insoluble nickel compounds as gradually as possible from the solution onto the carrier particles suspended therein. To this end, for example, a carrier suspension in a solution of a nickel-ammonia-complex is heated so as to allow the ammonia to escape, thereby causing the nickel to precipitate (cf. GB-A-926 235). Alternatively, urea is incorporated in the solution in which the carrier is suspended, after which the urea is decomposed by heating (cf. GB-A-1 220 105), causing the nickel hydroxide to precipitate. The aim of this very gradual precipitation of the nickel is to cover the carrier particles entirely or largely with nickel compound. Furthermore, GB-A-1 367 088 discloses the preparation of a catalyst by precipitating nickel on guhr, keeping temperature, pH, alkalinity and residence time within narrow ranges. In this process the nickel hydroxide is slowly precipitated from a diluted solution in a reaction vessel, after which the solid components are separated. Precipitation and post-reaction (the latter normally being referred to as "ageing") take place in the same reaction vessel, which therefore has to be relatively big, under the same reaction conditions or in two consecutive vessels in which the temperature is at least 90 °C in which the average residence time is at least 8 minutes.

It has now been found however that nickel-based hydrogenation catalysts containing 10 - 90 parts by weight of nickel/nickel compounds and 90 - 10 parts by weight of a water-insoluble carrier material, having an overall active nickel surface of 70 - 200 m² per gram of nickel and wherein the catalyst comprises nickel/nickel compound aggregates with an average particle size of 2 to 100 micrometers (µm), which process involves precipitation of nickel hydroxide/carbonate followed by ageing, separation, drying, and reduction of the precipitate in the presence of hydrogen can be prepared by a process in which in a first step a solution of a nickel salt and a solution of an alkaline compound are fed into a precipitation reactor and nickel hydroxide/carbonate is rapidly precipitated in the presence of at least part of the insoluble carrier material under vigorous agitation with a mechanical energy input of 5 - 25 kW per 1000 kg of solution in the precipitation reactor with a mean residence time of 0.01 - 1 minute, during which the normality of the solution in the precipitation reactor containing excess alkali, is kept between 0.1 and 0.3 N and the temperature is from 20 to 55 °C, and in which in a following step the reaction mixture is transferred to a post-reactor for ageing, in which the mean residence time is 20 to 180 minutes and the temperature is at least 10 °C higher than in the precipitation reactor and is kept between 60 and 100 °C, after which the solids are separated and further processed.

The nickel-based catalysts according to the present invention comprise a water-insoluble carrier material which is present or added during preparation. Suitable carrier materials are for example silica-containing materials such as kieselguhr, aluminium trioxide, and silicates such as bentonite. Kieselguhr is the preferred material, particularly kieselguhr containing from 50 to 90 wt.% of amorphous silica.

The carrier material can be added (a) directly as such, (b) as an aqueous suspension, (c) preferably as a suspension in an aqueous nickel salt solution, (d) as a suspension in an aqueous solution of the alkaline compound.

According to embodiments (a) - (d) the carrier can be added before or during precipitation. According to embodiments (a), (b) or (d), however, the carrier can also be added partly after precipitation, but also before or during ageing.

After precipitation and ageing according to the invention the solids are separated from the liquid, optionally washed, dried and activated by contacting them with hydrogen at an elevated temperature in a manner known per se.

Nickel compounds which can be used as starting materials for the preparation of the catalysts according to the present invention are water-soluble nickel compounds such as nitrate, sulphate, acetate and chloride. The solutions that are fed into the precipitation reactor preferably contain between 10 and 80 g nickel per litre; particularly preferred is the use of solutions containing between 25 and 60 g nickel per litre.

Alkaline compounds which can be used as starting material in the process according to the present invention are alkali metal hydroxides, alkali metal carbonate, alkali metal bicarbonate, the corresponding ammonium compounds and mixtures of the above-mentioned compounds. The concentration of the alkaline solution fed into the precipitation reactor is preferably 20-300 g of anhydrous material per litre (as far as the solubility permits this), particularly between 50 and 250 g per litre.

It has practical advantages to use the two solutions (nickel-containing and alkaline, respectively) in about equal concentrations expressed in equivalents, resulting in the use of about equal volumes.

The nickel-containing solution and the alkaline solution are fed at such rates that a slight excess of alkaline compound is present during the precipitation step, namely such that the normality of the liquid
 5 ranges from 0.1 to 0.3 (said normality being determined by titration with aqueous hydrochloric acid using methylorange as the indicator). In the ageing step it may sometimes be desirable to add further alkaline solution in order to maintain the alkalinity (normality) in the abovedefined range.

The precipitation reactor comprises a means for vigorous agitation of the reacting fluid and its dimensions are such in relation to the amounts of fluid fed that the short mean residence times indicated
 10 can be obtained. Mean residence times in the precipitation reactor are normally between 0.01 and 1 minute. The precipitation step and also the ageing step can be carried out batchwise, continuously and semi-continuously (e.g. according to the cascade method).

In the preferred continuous precipitation process (step i) the rate of addition of the solutions to the precipitation reactor is controlled by continuously or discontinuously measuring the alkalinity (normality) of
 15 the discharged liquid. This can sometimes also be done by monitoring the pH. Also the temperatures of the reacting liquids fed into the precipitation reactor are used to control the temperature at which precipitation takes place. The required vigorous agitation of the liquid in the precipitation reactor preferably takes place with an energy input of 5-25 K watts per 1000 kg of solution.

The reaction mixture obtained from the precipitation reactor is subsequently led into a significantly
 20 larger post-reactor, in which the liquid is further agitated. If desired, additional ingredients can be incorporated here such as carrier material, alkaline solution as defined hereinbefore and/or possibly promoters.

The temperature of the liquid in the postreactor, i.e. during the ageing step, is kept at a temperature between 60 and 100 °C, preferably between 90 and 98 °C.

The normality of the liquid in the post-reactor during the ageing step (step ii) is kept in the same range
 25 as during the precipitation step (step i); it may be required to add some further alkali. The ageing step can be performed in one or more post-reactors, the (overall) mean residence time being kept between 20 and 180 min. preferably between 60 and 150 min. If two or more postreactors are used it is desirable to arrange this in such a way that in the second or following post-reactor the temperature of the liquid is 10 to 15
 30 centigrades below the temperature in the first post-reactor.

After completion of the ageing step the solids are separated from the mother liquor, usually washed, dried, optionally ground and/or calcinated and subsequently activated with hydrogen gas at an elevated temperature usually ranging between 250 and 500 °, preferably between 300 and 400 °C. This activation can take place at atmospheric or higher pressure. Atmospheric pressure is preferred.

35 Preferably before drying, or during any previous step promoters can conveniently be added. Promoters comprise amounts of 0.05 to 10%, calculated on the weight of nickel, of metals/compounds such as copper, cobalt, zirconium, molybdenum, silver, magnesium, any other metals and combinations thereof.

The separated solid is preferably washed with water, sometimes made slightly alkaline, or water with a detergent added thereto.

40 Organic solvents can sometimes be used advantageously. Drying takes place preferably with forced air circulation. Spray-drying and freeze-drying are also quite well possible.

The present invention provides nickelbased catalysts which comprise 10.90 parts by weight of nickel/nickel compounds and 90-10 parts by weight of a water -insoluble carrier material, as well as 0-10, preferably 0.05-5-parts by weight of a metal promoter, which catalysts have an active nickel surface of 70-
 45 200 m²/g, preferably more than 100 m²/g, said catalysts further comprising aggregates which mainly consist of nickel/ nickel compounds with an average particle size of 2 to 100 micrometers μ m, preferably between 5 and 25 micrometers μ m, and which aggregates have an (outer) surface which is for at least 60% free of carrier particles attached thereto. Preferably the nickel/nickel compound aggregates have a surface which is for more than 80%, particularly for more than 90% free of carrier particles.

50 The nickel/nickel compound aggregates consist mainly, i.e. for more than 80%, preferably more than 90%, of nickel and nickel oxides, but some promoter material may also be present. These aggregates preferably contain nickel crystallites with an average diameter between 0.5 and 10, more particularly between 1 and 3 nanometers nm.

The catalyst according to the invention is used for the hydrogenation of unsaturated organic compounds, in particular oils and fats, fatty acid and derivatives thereof.

The invention is illustrated by the following Examples.

Example 1 (comparative example)

An aqueous suspension was prepared by suspending kieselguhr (containing 7.0% amorphous SiO₂) in a NiSO₄ solution (35 g Ni/l and 1.2 N), in such a way that the Ni:SiO₂-ratio was 1:2.3. Also an aqueous soda solution, containing 75 g of Na₂CO₃ (anh) per litre and 1.4 N, was prepared. Subsequently both solutions were continuously pumped into a vigorously agitated pump reactor, in about equal volumes, resulting in precipitation of nickelhydroxide/carbonate at a temperature of 80 °C. The alkalinity of the suspension so obtained was 0.096 N. In the reactor in which the precipitation took place the suspension had a residence time of 4 minutes, after which the suspension, was immediately passed to the first of a series of two postreactors. In each of these post-reactors the precipitate was aged for 50 minutes (mean residence time) at temperatures of 97 ° and 80 ° C, respectively. The aged precipitate was then continuously filtered off and the green filter cake thus obtained was washed with water, dried and activated with hydrogen under atmospheric pressure at a temperature of 350 ° C.

Electron microscopy and microrontgen analysis showed that the catalyst consisted of nickel crystallites averaging 2 nanometers (nm) and aggregates averaging 21 micrometers (μ). The surface of the nickel/nickel compound aggregates was for about 85% free of carrier particles and also the original shape of the siliceous skeletons was largely uncovered and well and freely perceptible.

Examples 2-7 (example 6 : comparative example).

Following the procedure as described in Example 1 further catalysts were prepared according to the invention, while varying the amounts and conditions, as is shown in Table I. Measures were taken to keep the other conditions unchanged.

In Table II, showing the hydrogenation characteristics of this catalyst, comparisons are made with a catalyst known from the literature.

On fatty acid hydrogenation it was found that for achieving a certain iodine value, with catalysts according to the invention less than half the hydrogenation time was sufficient and that in the case of fish oil the catalyst also retained its activity for a longer period. From the melting points it appeared that the new catalyst had a greater selectivity, i.e. less tri-saturated triglyceride was formed.

On fatty acid hydrogenation it turned out that hydrogenation could be carried through to lower iodine values in the same hydrogenation time and thus proceeded more rapidly than with the known catalyst used for comparison. Furthermore, the hydrogenations can also be performed with excellent results at a lower hydrogenation temperature. In addition, the new catalyst could be filtered very effectively, in any case better than the known catalyst.

Table III below gives an impression of fatty acid hydrogenation plotted against time (relation between iodine value and hydrogenation time under otherwise equal conditions).

TABLE III

Hydrogenation time (min)	Iodine value with catalyst 4 (Table II)	Iodine value with known catalyst (Table II)
30	45.1	72.1
60	15.3	45.5
90	9.8	22.2
120	5.3	17.8
150	3.3	15.1

Table III demonstrates that the iodine value of the hydrogenated fatty acid of about 15.2, obtained with the conventional catalyst widely used for this purpose after about 150 minutes, was already reached in about 60 minutes with the catalyst according to the invention, which is a considerable technological improvement.

TABLE I

Example:	1 (compar.)	2	3	4	5	6 (compar.)	7
Ni/SiO ₂ ratio Precipitation Conc. soda solution, mol/l Conc. nickel solution, mol/l Precipitation temp. (°C) Mean reaid. time (step 1), min Excess alkali (normality) Aging of precipitate Number of post-reactors Temperature (°C) Mean reaid. time (step 2) in minutes Excess alkali (mol/l) * - extra alkali	2.3 0.7 0.6 80 4 0.10 2 97/80 50/50 0.135/ 0.192*	2.3 0.7 0.6 20 1 0.19 2 97/80 50/50 --	2.3 0.7 0.6 30 1 0.21 1 96 50 --	2.3 0.7 0.6 55 1 0.22 2 93/80 50/50 --	2.3 0.7 0.6 50 1 0.21 2 90/77 05/50 --	1.8 0.7 0.6 85 0.3 0.13 1 95 30 --	1.0 1.0 0.6 22 0.5 0.21 1 97 30 --

Catalysts 1-5 contained 70% nickel and 30% SiO₂;
 catalysts 6 and 7 contained 64% nickel and 36% SiO₂.

Active nickel surfaces ranged between 120 and 150 m²/g nickel.

Nickel aggregates were found to range between 9 and 26 micrometers (nm) and the catalyst of Example 4 was shown to have nickel aggregates the surface of which proved to be for 85% free of carrier particles.

TABLE II

Example	1 (compar. ex.)	2	3	4	5	6 (compar. ex.)	7	Compar. example
Ni & in reduced catalyst Oil hydrogen. test refined marine oil of I.V. 165 to 85, conditions: 250 g oil, 0.18 Ni on oil, 60LH ₂ /h press, 1 bar, max. temp. 180°C, 750 rpm, reduct. temp. of cat. 350°C Hydrogen. time (min) m.p. of oil (°C) fatty acid hydrog. test 300 g tallow fatty acid (olein fraction) 0.07 Ni on fatty acid, H ₂ press. 30 bar max. temp. 180°C stirring speed 850 rpm hydrog. time 150 min reduction cat. 350°C I.V. after hydr.	52.4	51.0	52.6	53.0	52.7	51.2	52.0	22 (in fat susp.)
	92 32	85 32.5	83 32	92 32.5	85 32.5	90 33	103 32.5	127 36
	3.1	2.5	3.2	3.3	2.6	3.4	3.0	15.1

Example 8

A 10% aqueous soda solution and a 3.5% aqueous nickel sulphate (calculated as nickel) solution in which kieselguhr (22 g per litre) had been blended were both continuously pumped into a small precipitation reactor (75 ml capacity) whilst the reactor was heavily agitated (energy input 6 Watts per litre

of solution). The two liquids were fed into the reactor in such rates that the pH in the precipitation reactor was 9.3. The residence time was 0.5 minutes.

After precipitation the slurry contained about 4% of solids and this slurry was continuously aged in a relatively larger vessel (capacity 4.5 l) with moderate stirring. The ageing temperature was 97 °C and the pH was 8.9. The average residence time in the ageing reactor was about 30 minutes.

After 1.5 hours the flows were stopped and 4.5 l of slurry were filtered in a Büchner funnel under vacuum. After filtration the solids (filter cake) were washed with 4 litres of distilled water. The filter cake was then dried overnight in an oven at 120 °C.

Samples of the green filter cake were investigated by electron microscopy (magnification 500 and 1000 x). The photos showed small nickel/nickel compound aggregates of which 80% were free of carrier particles and also the original shapes of the siliceous skeletons were largely uncovered by nickel/nickel compounds and freely perceptible.

The green cakes were reduced at 400 °C with a hydrogen flow of 15 N (S:T:P) m³/kg Ni for 30 minutes.

The active nickel surface area was determined by hydrogen chemisorption and yielded a value of 110 m²/g nickel. The average size of the nickel crystallites was calculated to be 3 nanometers (nm) and the size of the nickel/nickel compound aggregates was found to be 30 micrometers (μm).

This catalyst had excellent properties for the hydrogenation of soybean and fish oils.

Claims

1. A process for preparing a nickel-based hydrogenation catalyst containing 10 - 90 parts by weight of nickel/nickel compounds and 90 - 10 parts by weight of a water-insoluble carrier material, having an overall active nickel surface of 70 - 200 m² per gram of nickel and wherein the catalyst comprises nickel/nickel compound aggregates with an average particle size of 2 to 100 micrometers (μm), which process involves precipitation of nickel hydroxide/carbonate followed by ageing, separation, drying, and reduction of the precipitate in the presence of hydrogen, characterized in that in a first step a solution of a nickel salt and a solution of an alkaline compound are fed into a precipitation reactor and nickel hydroxide/carbonate is rapidly precipitated in the presence of at least part of the insoluble carrier material under vigorous agitation with a mechanical energy input of 5 - 25 kW per 1000 kg of solution in the precipitation reactor with a mean residence time of 0.01 - 1 minute, during which the normality of the solution in the precipitation reactor containing excess alkali, is kept between 0.1 and 0.3 N and the temperature is from 20 to 55 °C, and that in a following step the reaction mixture is transferred to a post-reactor for ageing, in which the mean residence time is 20 to 180 minutes and the temperature is at least 10 °C higher than in the precipitation reactor and is kept between 60 and 100 °C, after which the solids are separated and further processed.
2. A process according to claim 1, characterized in that the temperature in the post-reactor is kept between 90 and 98 °C.
3. A process according to any one of claims 1 to 2, characterized in that the solution of the nickel salt fed into the precipitation reactor contains 10 - 80 g nickel per litre.
4. A process according to any one of claims 1 to 3, characterized in that the nickel salt is a salt of a mineral acid.
5. A process according to any one of claims 1 to 4, characterized in that the solution of the alkaline compound fed into the precipitation reactor contains 30 to 300 g of anhydrous alkaline compound per litre.
6. A process according to any one of claims 1 to 5, characterized in that the solution of the alkaline compound contains sodium carbonate.
7. A process according to any of claims 1 to 6, characterized in that silica is used as the water-insoluble carrier material.
8. A process according to claim 7, characterized in that as a water-insoluble carrier material kieselguhr is used consisting for 50 to 90 % of amorphous SiO₂.

9. A process according to any one of claims 1 to 8, characterized in that kieselguhr is added in an amount of 20 to 200 g per litre.
10. A process according to any one of claims 1 to 9, characterized in that activation of the catalyst is carried out with hydrogen at a temperature between 250 and 500 °C, preferably between 300 and 400 °C.
11. A process according to any one of claims 1 to 10, characterized in that precipitation is carried out continuously by dosing a kieselguhr suspension in an aqueous nickel salt solution together with an alkaline solution in a small, vigorously rotating mixing pump and subsequently pumping the suspension into one or more post-reactors.
12. A process according to claim 11, characterized in that two or more post-reactors are used, the temperature in the second and any following post-reactor being 5 - 15 °C lower than in the first post-reactor.

Patentansprüche

1. Verfahren zum Herstellen eines auf Nickel basierenden Hydrierungskatalysators, der 10 bis 90 Gewichtsteile Nickel/Nickelverbindungen und 90 bis 10 Gewichtsteile eines wasserunlöslichen Trägermaterials enthält und eine aktive Nickeloberfläche von insgesamt 70 bis 200 m² pro Gramm Nickel aufweist, wobei der Katalysator Nickel/Nickelverbindung-Aggregate mit einer durchschnittlichen Teilchengröße von 2 bis 100 Mikrometer (µm) umfaßt und wobei das Verfahren das Ausfällen von Nickelhydroxid/carbonat und nachfolgendes Altern, Abtrennen, Trocknen und Reduzieren der Fällung in Gegenwart von Wasserstoff beinhaltet, dadurch gekennzeichnet, daß in einer ersten Stufe eine Lösung eines Nickelsalzes und eine Lösung einer alkalischen Verbindung in einen Fällungsreaktor eingespeist werden und in Gegenwart mindestens eines Teils des unlöslichen Trägermaterials unter kräftigem Rühren mit einer Zufuhr von mechanischer Energie von 5 bis 25 kW pro 1000 kg Lösung in dem Fällungsreaktor mit einer mittleren Verweilzeit von 0,01 bis 1 Minute Nickelhydroxid/carbonat rasch ausgefällt wird, während die Normalität der Lösung in dem überschüssigen Alkali enthaltenden Fällungsreaktor zwischen 0,1 und 0,3 n gehalten wird und die Temperatur 20 bis 55 °C beträgt, und in einer folgenden Stufe das Reaktionsgemisch zum Altern in einen Nachreaktor überführt wird, in dem die mittlere Verweilzeit 20 bis 180 Minuten beträgt und die Temperatur um mindestens 10 °C höher liegt als in dem Fällungsreaktor sowie zwischen 60 und 100 °C gehalten wird, wonach die Feststoffe abgetrennt und weiterverarbeitet werden.
2. Verfahren nach Anspruch 1, dadurch gekennzeichnet, daß die Temperatur in dem Nachreaktor zwischen 90 und 98 °C gehalten wird.
3. Verfahren nach Anspruch 1 oder 2, dadurch gekennzeichnet, daß die in den Fällungsreaktor eingespeiste Lösung das Nickelsalzes 10 bis 80g Nickel pro Liter enthält.
4. Verfahren nach einem der Ansprüche 1 bis 3, dadurch gekennzeichnet, daß das Nickelsalz ein Salz einer Mineralsäure ist.
5. Verfahren nach einem der Ansprüche 1 bis 4, dadurch gekennzeichnet, daß die in den Fällungsreaktor eingespeiste Lösung der alkalischen Verbindung 30 bis 300 g wasserfreie alkalische Verbindung pro Liter enthält.
6. Verfahren nach einem der Ansprüche 1 bis 5, dadurch gekennzeichnet, daß die Lösung der alkalischen Verbindung Natriumcarbonat enthält.
7. Verfahren nach einem der Ansprüche 1 bis 6, dadurch gekennzeichnet, daß als wasserunlösliches Trägermaterial Siliciumdioxid verwendet wird.
8. Verfahren nach Anspruch 7, dadurch gekennzeichnet, daß als wasserunlösliches Trägermaterial Kieselgur, der zu 50 bis 90 % aus amorphem SiO₂ besteht, verwendet wird.

9. Verfahren nach einem der Ansprüche 1 bis 8, dadurch gekennzeichnet, daß Kieselgur in Mengen von 20 bis 200 g pro Liter zugegeben wird.
- 5 10. Verfahren nach einem der Ansprüche 1 bis 9, dadurch gekennzeichnet, daß die Aktivierung des Katalysators mit Wasserstoff mit einer Temperatur zwischen 250 und 500 °C, vorzugsweise zwischen 300 und 400 °C, durchgeführt wird.
- 10 11. Verfahren nach einem der Ansprüche 1 bis 10, dadurch gekennzeichnet, daß die Fällung durch Dosieren einer Kieselgursuspension in einer wäßrigen Nickelsalzlösung zusammen mit einer alkalischen Lösung in einer kleinen, kräftig rotierenden Mischpumpe und nachfolgendes Einpumpen der Suspension in einen oder mehrere Nachreaktoren kontinuierlich durchgeführt wird.
12. Verfahren nach Anspruch 11, dadurch gekennzeichnet, daß zwei oder mehr Nachreaktoren verwendet werden, wobei die Temperatur im zweiten und in jedem folgenden Nachreaktor um 5 bis 15 °C
15 niedriger ist als im ersten Nachreaktor.

Revendications

- 20 1. Procédé de préparation d'un catalyseur d'hydrogénation à base de nickel contenant 10-90 parties en poids de nickel/composé de nickel et 90-10 parties en poids d'un véhicule insoluble dans l'eau, ayant une surface globale de nickel actif de 70-200 m²/g de nickel et dans lequel le catalyseur comprend des agrégats de nickel/composé de nickel d'une dimension moyenne de particule de 2 à 100 micromètres (µm), lequel procédé de préparation implique la précipitation de l'hydroxyde de nickel/carbonate suivie par le vieillissement, la séparation, le séchage et la réduction du précipité en présence d'hydrogène,
25 caractérisé en ce que dans une première étape une solution d'un sel de nickel et une solution d'un composé alcalin sont introduits dans un réacteur de précipitation et l'hydroxyde de nickel/carbonate est rapidement précipité en présence d'au moins une partie du véhicule insoluble sous agitation vigoureuse avec l'apport d'une énergie mécanique de 5-25 kW par 1000 kg de solution dans le réacteur de précipitation avec un temps de séjour moyen de 0.01-1 minute pendant lequel la normalité de la
30 solution dans le réacteur de précipitation contenant l'excès alcalin, est maintenue entre 0.1 et 0.3 N et la température est comprise entre 20 et 55 °C, et en ce que dans une étape ultérieure, le mélange réactionnel est transféré à un post-réacteur pour vieillissement, dans lequel le temps de séjour moyen est de 20 à 180 minutes et la température est supérieure d'au moins 10 °C à celle du réacteur de précipitation et est maintenue entre 60 et 100 °C, après quoi les solides sont séparés et ensuite mis en
35 oeuvre.
2. Procédé selon la revendication 1, caractérisé en ce que la température dans le post-réacteur est maintenue entre 90 et 98 °C.
- 40 3. Procédé selon l'une des revendications 1 ou 2, caractérisé en ce que la solution de sel de nickel introduite dans le réacteur de précipitation contient 10-80 g de nickel/litre.
4. Procédé selon l'une des revendications 1 à 3, caractérisé en ce que le sel de nickel est un sel d'un acide minéral.
- 45 5. Procédé selon l'une des revendications 1 à 4, caractérisé en ce que la solution de composé alcalin introduite dans le réacteur de précipitation contient 30 à 300 g de composé alcalin anhydre par litre.
6. Procédé selon l'une des revendications 1 à 5, caractérisé en ce que la solution de composé alcalin
50 contient du carbonate de sodium.
7. Procédé selon l'une des revendications 1 à 6, caractérisé en ce que la silice est utilisée en tant que véhicule insoluble dans l'eau.
- 55 8. Procédé selon la revendication 7, caractérisé en ce que le véhicule inerte et insoluble dans l'eau est le kieselguhr consistant en 50 à 90 % de silice amorphe.

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9. Procédé selon l'une des revendications 1 à 8, caractérisé en ce que ce kieselguhr est additionné dans une quantité de 20 à 200 g/litre.
- 5 10. Procédé selon l'une des revendications 1 à 9, caractérisé en ce que l'activation du catalyseur est effectuée en présence d'hydrogène à une température entre 250 et 500 °C, de préférence entre 300 et 400 °C.
- 10 11. Procédé selon l'une des revendications 1 à 10, caractérisé en ce que la précipitation est effectuée de façon continue en dosant une suspension de kieselguhr dans une solution de sel de nickel aqueux en association avec une solution alcaline dans une petite pompe de mélange en rotation vigoureuse et subséquentement en pompant la suspension dans un ou plusieurs post-réacteurs.
- 15 12. Procédé selon la revendication 11, caractérisé en ce que deux ou plusieurs post-réacteurs sont utilisés, la température dans le second et tous les post-réacteurs suivants étant de 5-15 °C inférieurs à celle du premier réacteur.

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